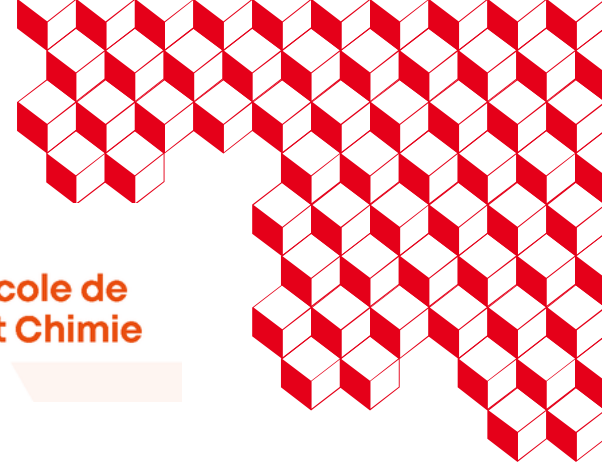




liten



GePhyX Grenoble École de  
Physique et Chimie



# Valoriser le CO<sub>2</sub> par réduction en carburants et intermédiaires chimiques

Quels enjeux et quelles technologies ?

Alban CHAPPAZ and Isabelle ROUGEAUX



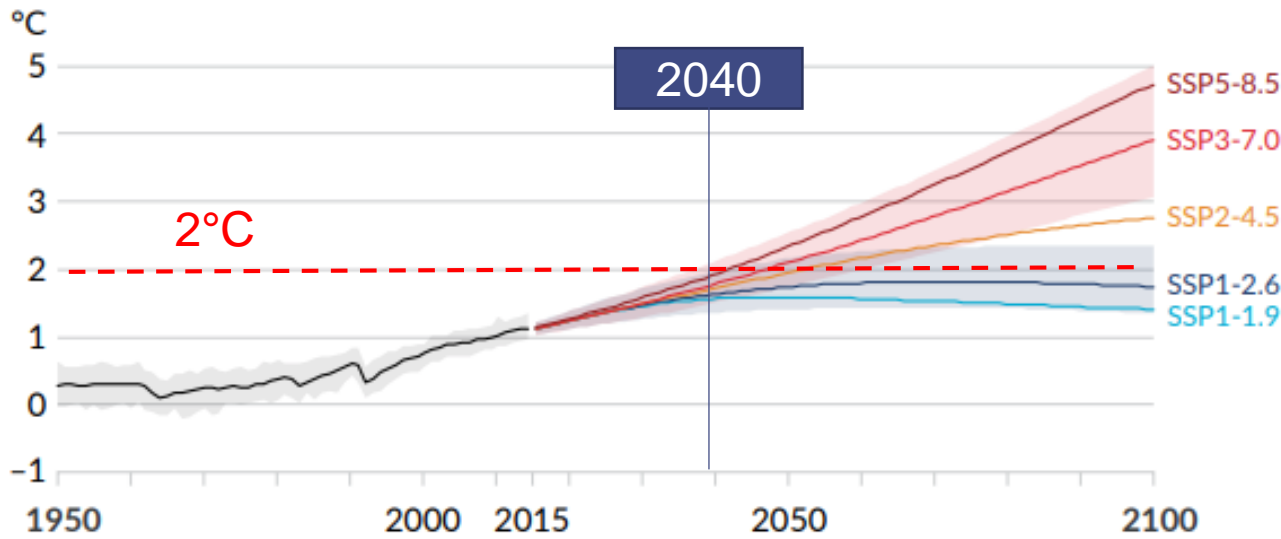
## **Context overview**

- 1 Electro-catalytic reduction**
- 2 Thermo-catalytic reduction**
- 3 Case study**

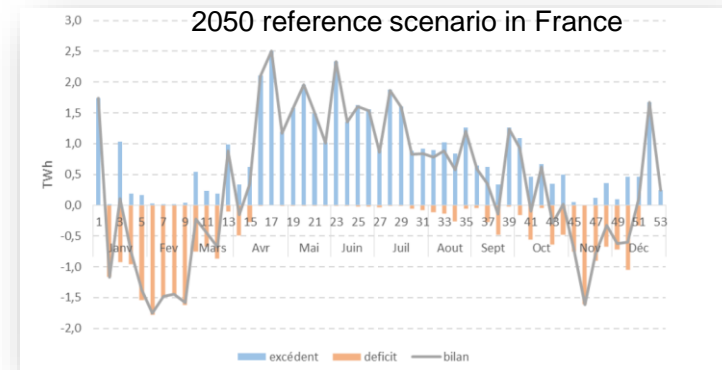
# The energy transition and CO<sub>2</sub> mitigation

Increase of the greenhouse gases (GHG) concentration in the atmosphere → increase of mean surface temperature

- **Energy transition:** fossil fuels → renewable sources
- **CO<sub>2</sub> capture** and storage (CCS) or utilization (CCU)



IPCC, 2021: *Climate Change 2021: The Physical Science Basis.*



Etude portant sur l'hydrogène et la méthanation, E&E Consultant, Solagro, 2014

Global warming is likely to reach **2°C before 2040** if no changes are made



**Intermittent nature** of renewable energies

## Targets

reduce by 50% the global greenhouse gas emissions over the next ten years

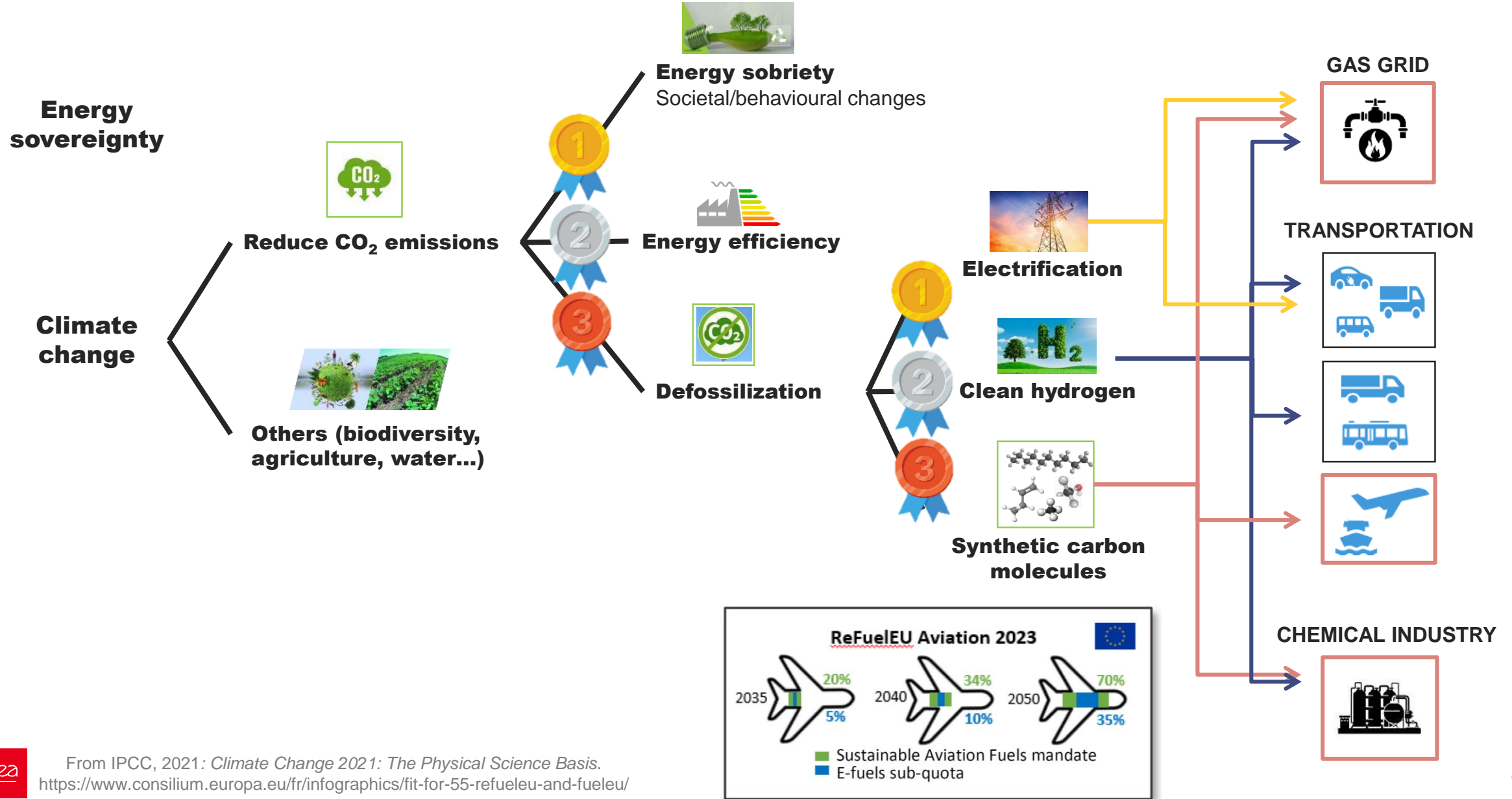


Need to **install decarbonized electric sources**

Need to **store the excess electricity** into other forms of energy

IPCC, 2021: *Climate Change 2021: The Physical Science Basis.*

# Prioritization of solutions for climate change



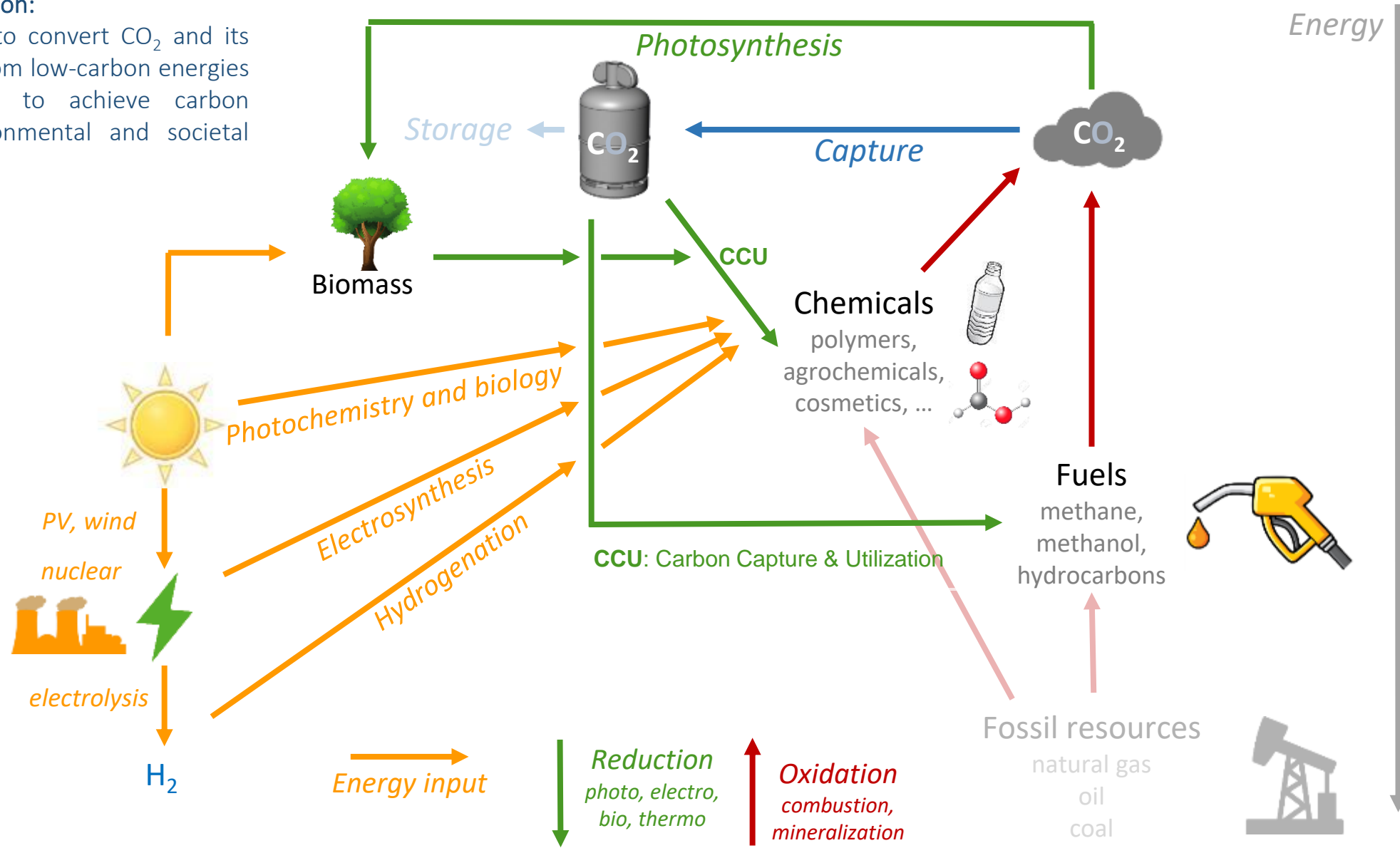
# From linear towards circular carbon economy



A Carbon Circular Economy is based on: a collection of technologies able to convert CO<sub>2</sub> and its derivatives into useful products, from low-carbon energies (incl. nuclear and renewables), to achieve carbon neutrality with a positive environmental and societal impact.

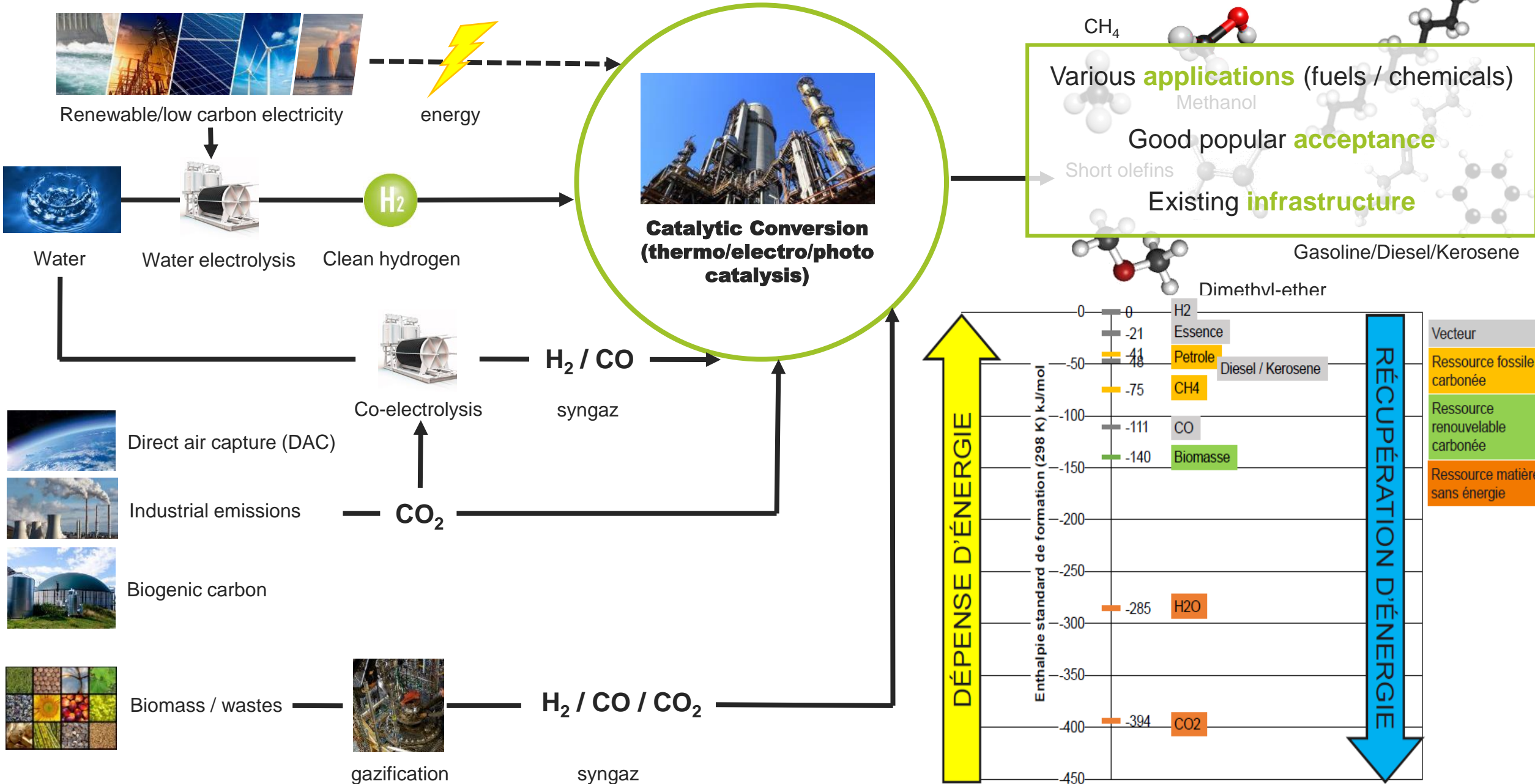
**Cross-cutting challenges**

- Impact analysis of soils and climate
- Multicriterai Life Cycle Analyses
- Sustainability of resources



# Catalytic conversion technologies

Liquid and gaseous carbon-containing molecules



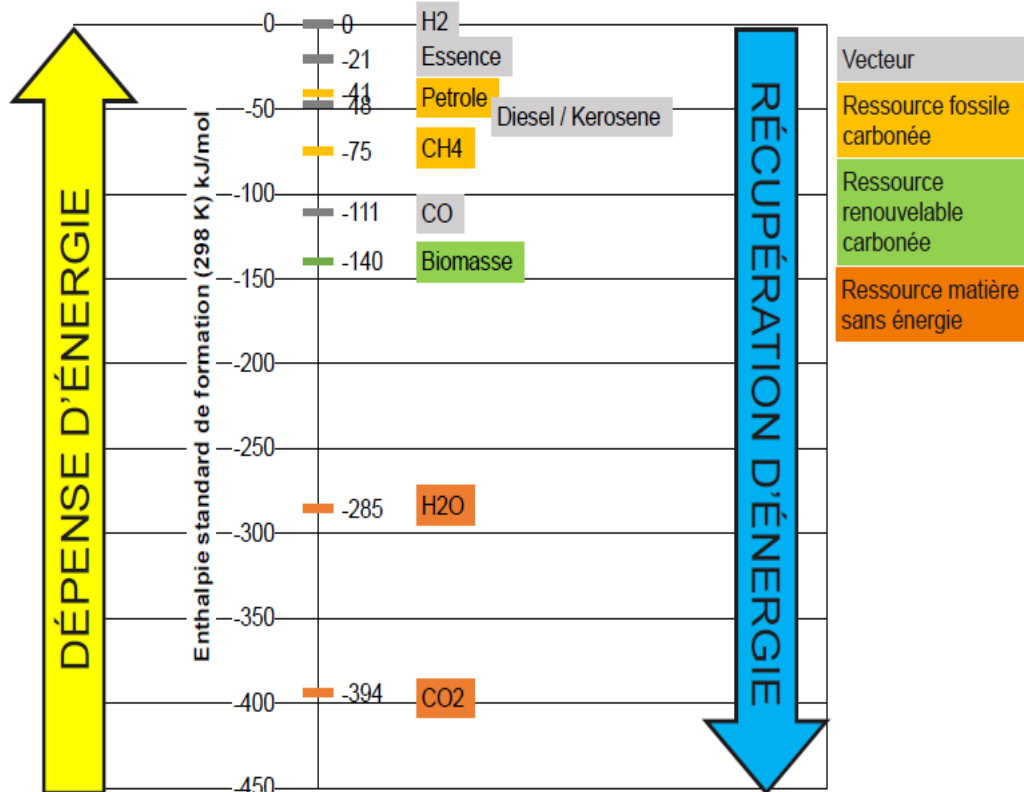
Various **applications** (fuels / chemicals)

Methanol

Good popular **acceptance**

Short olefins

Existing **infrastructure**



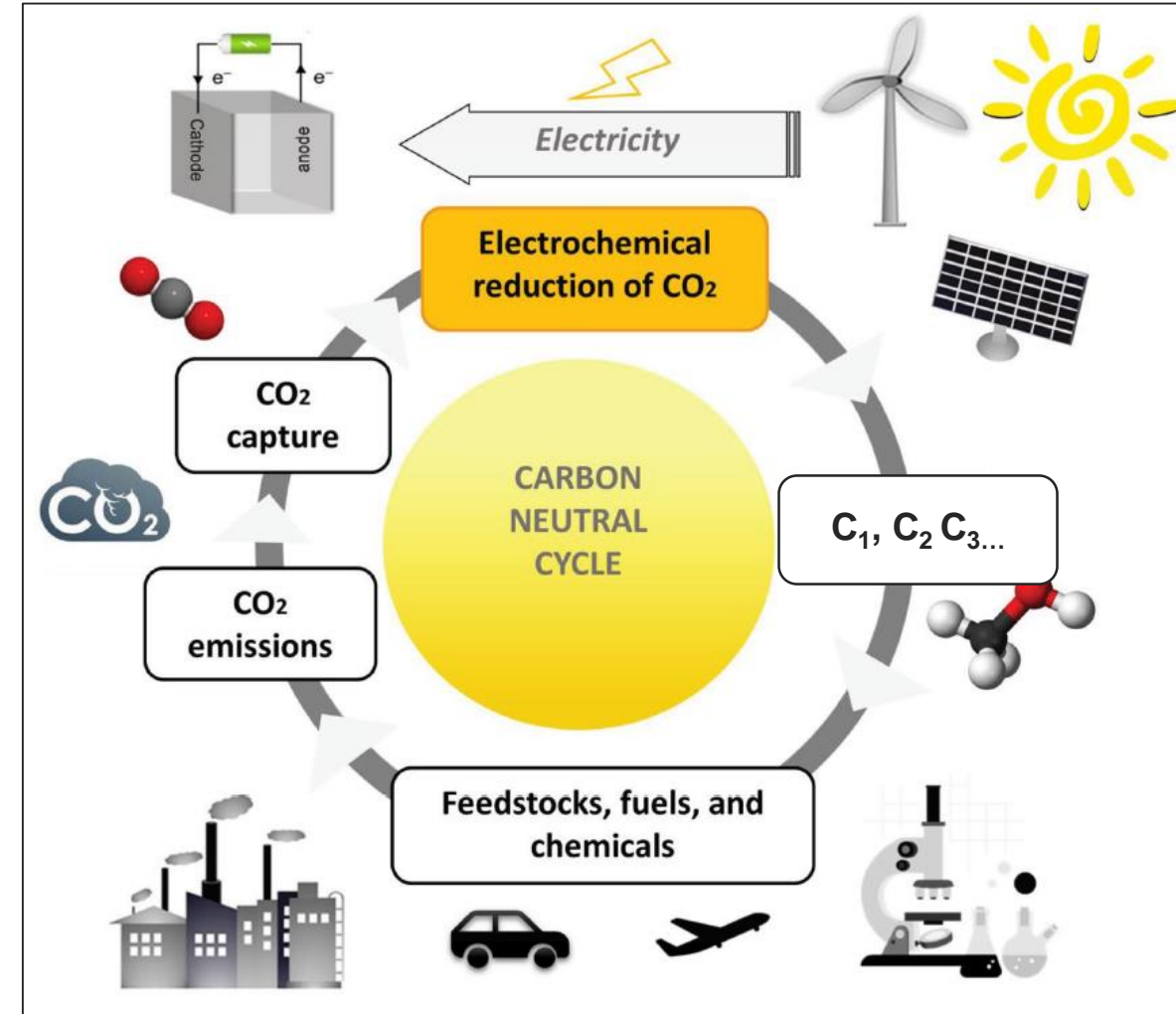


# **1 ■ Electro-catalytic reduction**

# OVERVIEW ON ELECTROCHEMICAL CO<sub>2</sub> REDUCTION REACTION (CO<sub>2</sub>RR)



- Novel research field towards :
  - A CO<sub>2</sub>-neutral global economy / Circular Carbon Economy
  - Combating fast accelerating and disastrous climate changes
  - New solutions to store renewable energy in value-added chemicals and fuels
- CO<sub>2</sub> capture : Industrial fumes or DAC (Direct Air Capture)
- Powering electrochemical cells with renewable energies





# ELECTROCHEMICAL REACTIONS

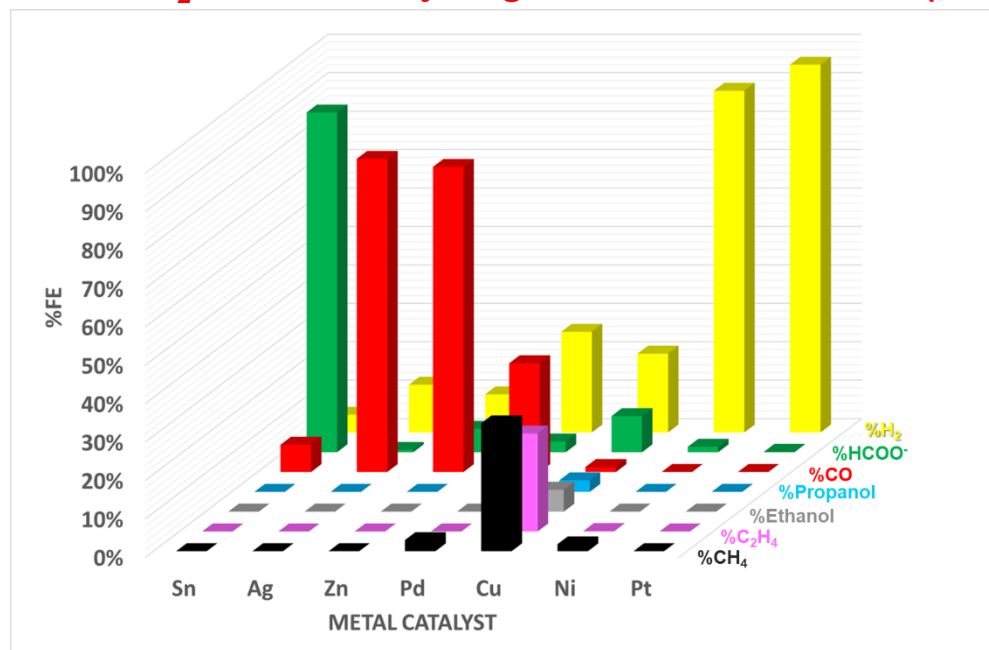


## Cathode :

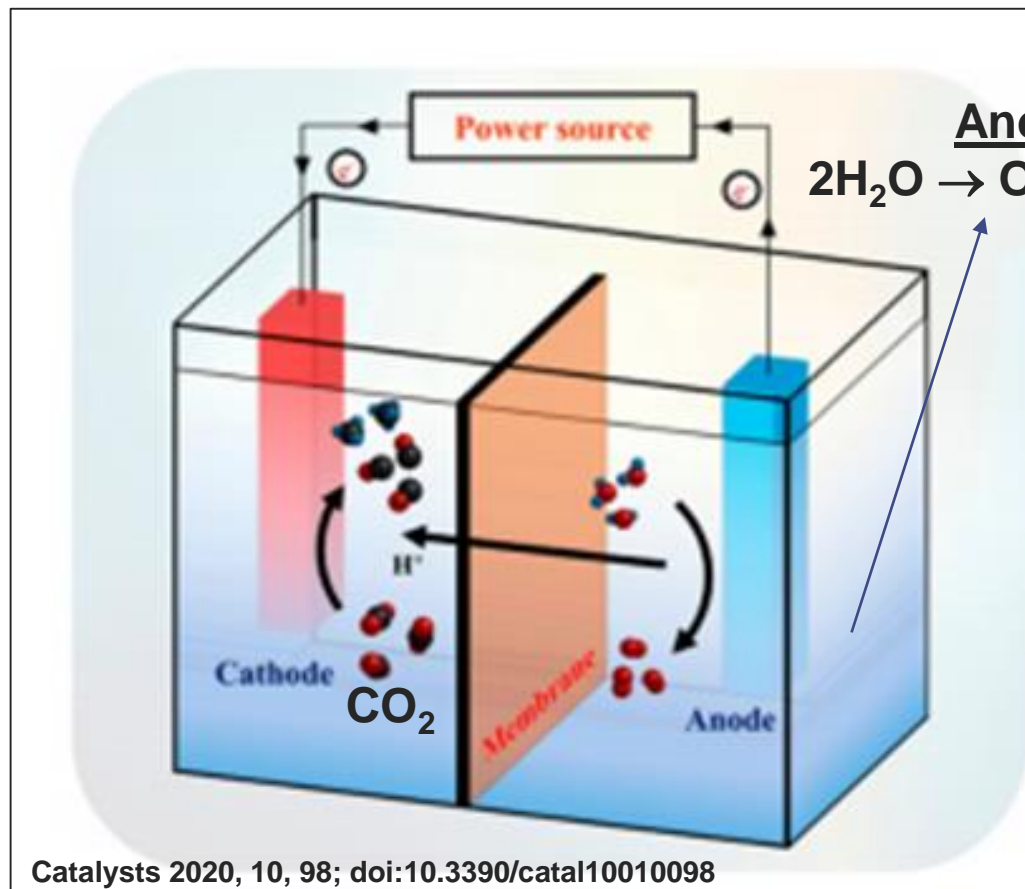
Several possible reactions :

| Half-Electrochemical Thermodynamic Reactions                                                        | Product                       | E° Redox |
|-----------------------------------------------------------------------------------------------------|-------------------------------|----------|
| $\text{CO}_2 + \text{e}^- \rightarrow \text{CO}_2^\bullet$                                          | CO <sub>2</sub> anion radical | -1.90 V  |
| $\text{CO}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow \text{HCOOH}$                                  | Formic acid                   | -0.61 V  |
| $\text{CO}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow \text{CO} + \text{H}_2\text{O}$                | Carbon monoxide               | -0.53 V  |
| $\text{CO}_2 + 4\text{H}^+ + 4\text{e}^- \rightarrow \text{HCHO} + \text{H}_2\text{O}$              | Formaldehyde                  | -0.48 V  |
| $\text{CO}_2 + 6\text{H}^+ + 6\text{e}^- \rightarrow \text{CH}_3\text{OH} + \text{H}_2\text{O}$     | Methanol                      | -0.38 V  |
| $\text{CO}_2 + 8\text{H}^+ + 8\text{e}^- \rightarrow \text{CH}_4 + 2\text{H}_2\text{O}$             | Methane                       | -0.24 V  |
| $2\text{CO}_2 + 12\text{H}^+ + 12\text{e}^- \rightarrow \text{C}_2\text{H}_4 + 4\text{H}_2\text{O}$ | Ethylene                      | -0.41 V  |

$2\text{H}^+ + 2\text{e}^- \rightarrow \text{H}_2$  : Parasitic Hydrogen Evolution Reaction (HER)



Chem. Rev.2019, 119, 7610–7672

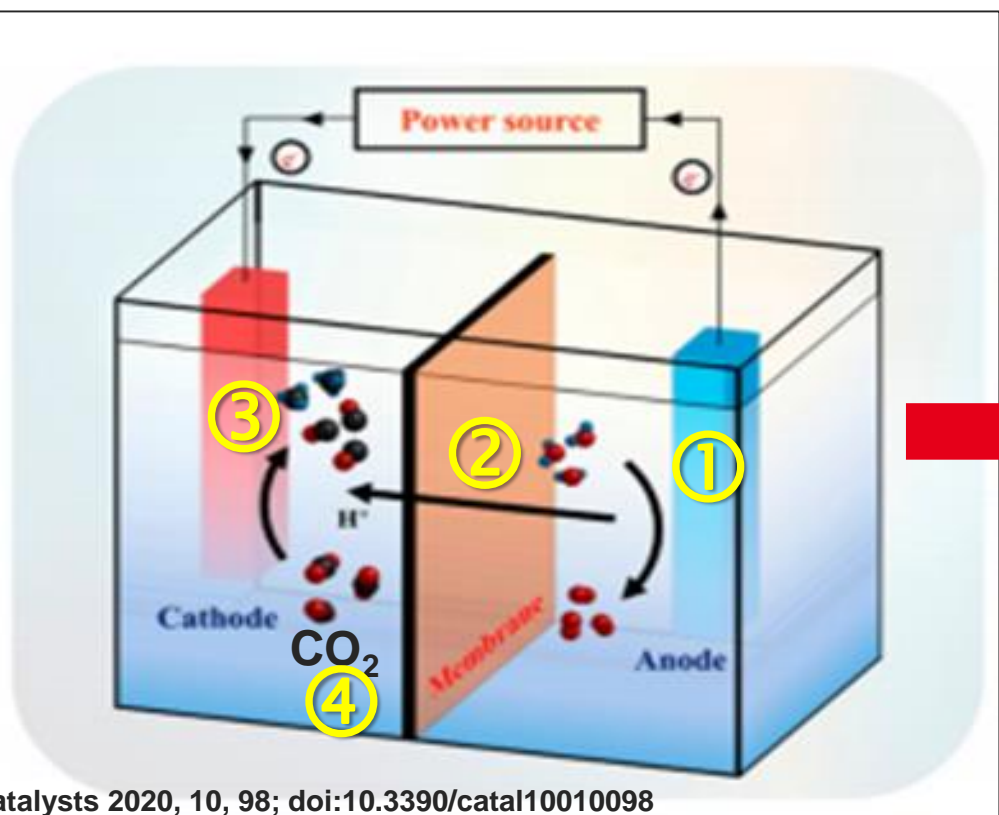


- Mild reaction conditions (suitable with intermittent energy)

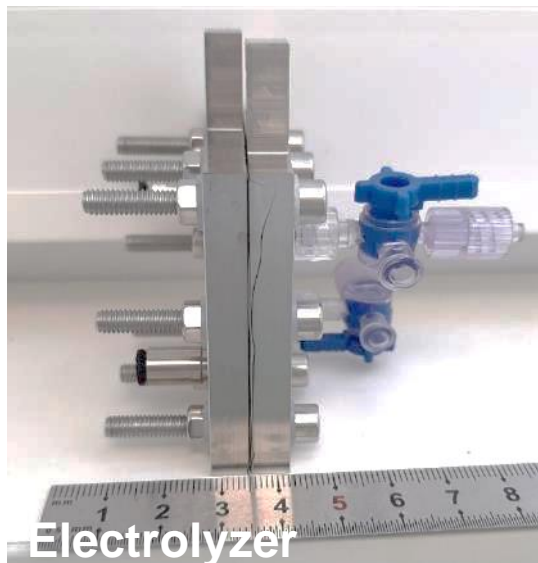


- Flexible and controllable process by different parameters (electrode materials, electrolytes and applied potentials)

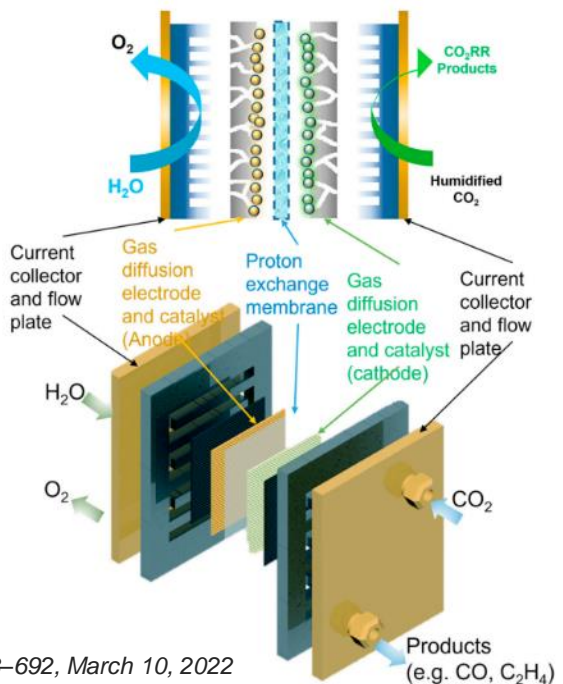
# CO2RR INDUSTRIALIZATION



Catalysts 2020, 10, 98; doi:10.3390/catal10010098



Electrolyzer



• Need to optimize :

- ① Anodic materials
- ② Membrane
- ③ Cathodic materials
- ④ CO<sub>2</sub> feeding

⇒ High Current density / High energy efficiency

⇒ High CO<sub>2</sub> conversion

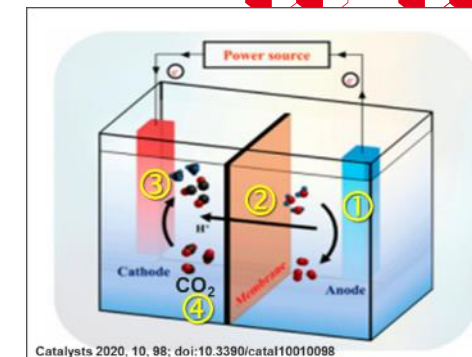
⇒ Long term stability

⇒ Good selectivity



# PARAMETERS TO OPTIMIZE FOR INDUSTRIALIZATION

- ① • Anodic catalysts : Expensive materials (Iridium, Platinum ...)
  - ⇒ Need to be replaced by lower cost materials



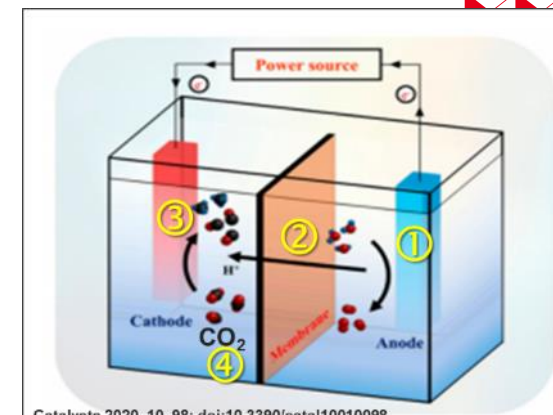
- ② • Membrane : How to select the suitable polymer?

|                                                 | Cationic | Anionic | Bi-Polar                        |
|-------------------------------------------------|----------|---------|---------------------------------|
| Performances<br>(conductivity, current density) | ☺        | ☹       | ☺                               |
| HER                                             | ☹        | ☺       | ☺                               |
| Stability                                       | ☺        | ☹       | ☺                               |
| Cost                                            | ☹        | ☺       | ☹ <i>Not currently marketed</i> |

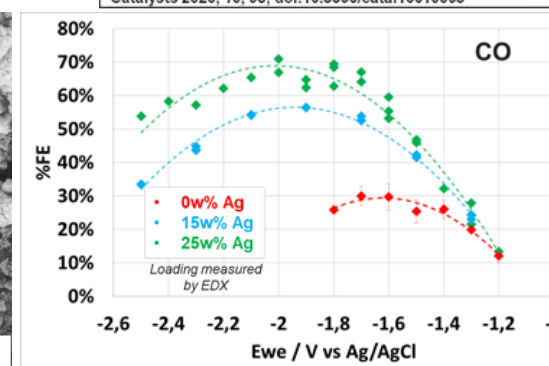
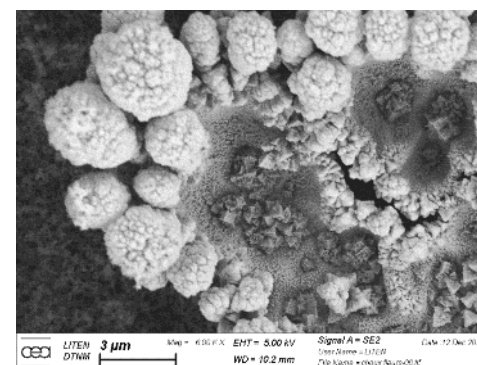
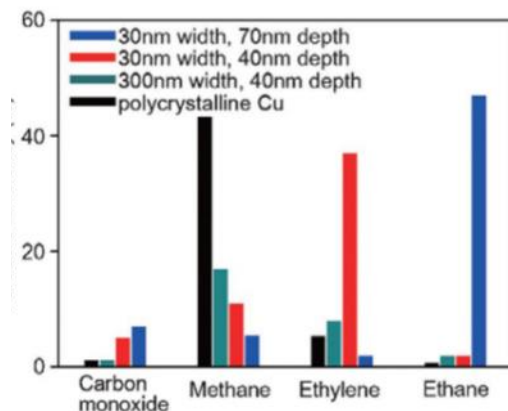
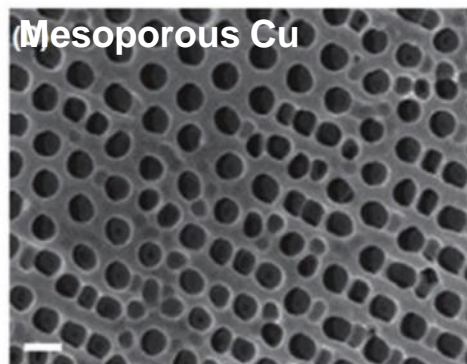
# PARAMETERS TO OPTIMIZE FOR INDUSTRIALIZATION

## ③ • Cathodic materials :

- **Catalysts** : Influence of the nature and the morphological structure of the catalyst on the product obtained, the rate of the reaction and the selectivity
- ⇒ **Need specific synthesis way / no directly commercially available**

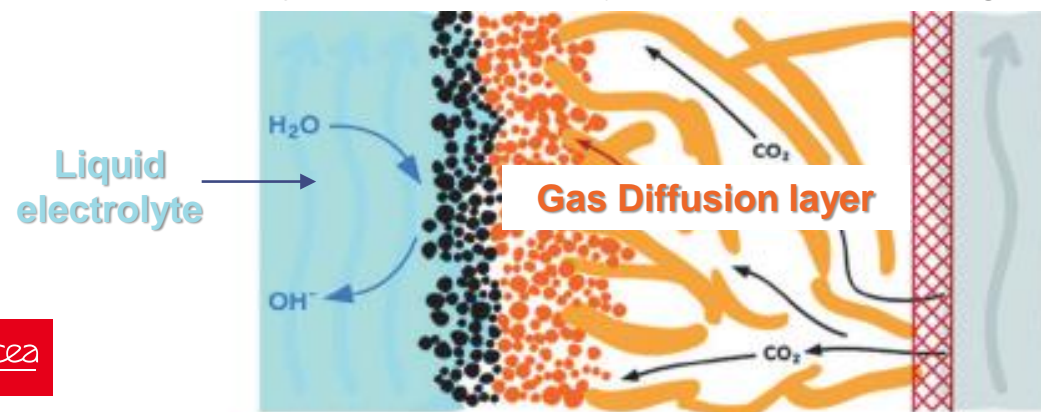


Catalysts 2020, 10, 98; doi:10.3390/catal10010098



DOI: 10.1002/ese3.935

- **Catalyst support** : Key role to control the gas and water diffusion



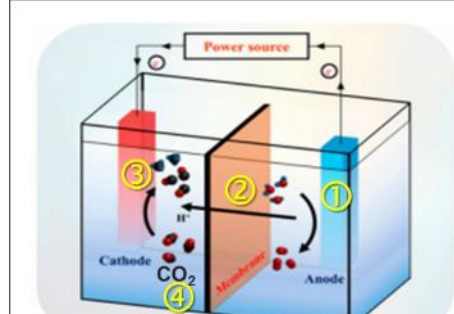
- **Catalyst**
- **Carbon Powder**
- **Carbon Fiber**



# PARAMETERS TO OPTIMIZE FOR INDUSTRIALIZATION

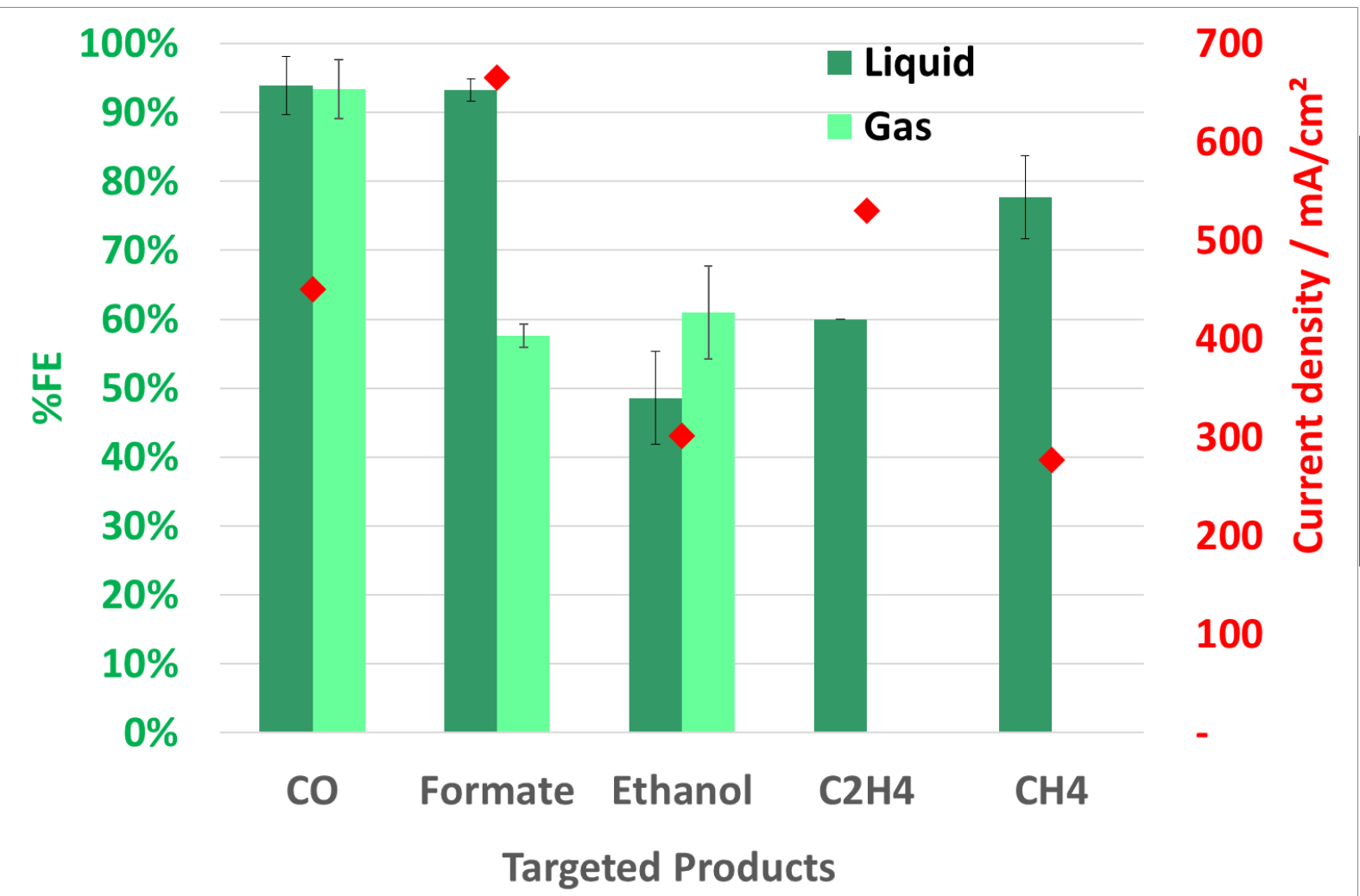


- ④ • CO<sub>2</sub> feeding : It depends on the design of electrolyzer



|                   | Gaseous CO <sub>2</sub>                                                                                                                                                                                                                                     | CO <sub>2</sub> dissolved in liquid                                                                                                                                                                                                                                |
|-------------------|-------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|--------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|
|                   |                                                                                                                                                                                                                                                             |                                                                                                                                                                                                                                                                    |
| <b>Advantages</b> | <ul style="list-style-type: none"> <li>- No CO<sub>2</sub> capture step required</li> <li>- No electrolyte required</li> <li>- High concentration of CO<sub>2</sub> on the catalyst ⇒ High reaction rate (current) ⇒ Rapid diffusion through GDL</li> </ul> | <p>CO<sub>2</sub> capture + Electro-reduction in 1 single step</p>                                                                                                                                                                                                 |
| <b>Drawbacks</b>  | <p>Need to pressurize cathodic compartment</p>                                                                                                                                                                                                              | <ul style="list-style-type: none"> <li>- CO<sub>2</sub> must be dissolved in electrolyte with high CO<sub>2</sub> capacity : Aqueous solution, Ionic liquid (but expensive)</li> <li>- Reaction limited by the supply of CO<sub>2</sub> to the catalyst</li> </ul> |

# RECENT ELECTROLYZER PERFORMANCES



- High current densities
- Good selectivity
- High %FE for C<sub>1</sub> (CO, Formate and CH<sub>4</sub>)
- Limited performances for complex molecules (>C<sub>2</sub>)

# CONCLUSIONS



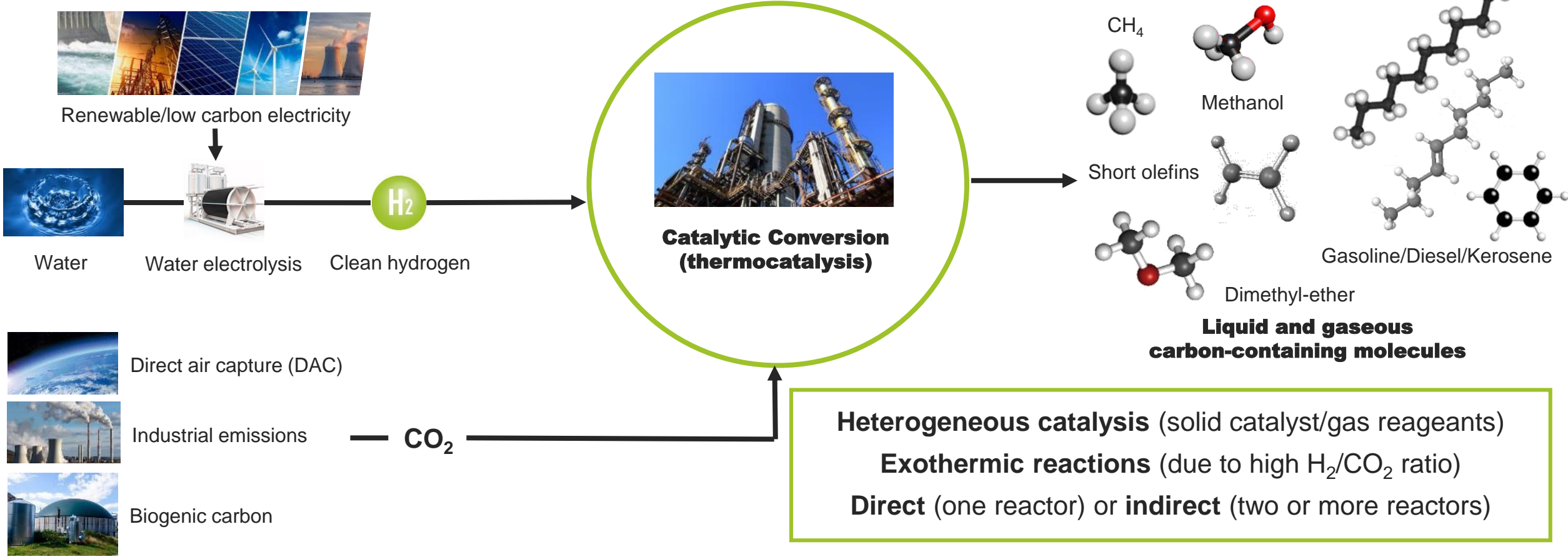
- **CO<sub>2</sub>RR to high value-added chemicals** ⇒ **Promising technology to achieve sustainable carbon neutralization**
- **Interesting results for :**
  - C<sub>1</sub> : possibility to be further chemically converted to important chemicals (acids, alcohols, and olefins)
  - C<sub>2</sub> : directly synthesized with complex catalysts (Ethanol, Ethylene ...)
- **But it seems difficult to obtain molecules beyond C<sub>3</sub>**
- **No H<sub>2</sub> needed → Safety aspect**
- **Flexibility of the technology (compatibility with intermittent energy)**
- **Actual TRL : 4-5 (>7 : *industrialization*) → Many optimizations still required**
- **Emerging companies : OPUS-12, Dioxide Materials, DNV, CO<sub>2</sub> CERT, Siemens and CarbonEnergy**



# **2** ■ **Thermocatalytic CO<sub>2</sub> reduction**



# Thermocatalytic conversion technologies



**Methanation (Sabatier) – TRL = 9**



→ **Thermodynamic control**  
(equilibrium X~95% at 350°C, 5 bar)

→ **High kinetics** (Ni or Ru catalysts)

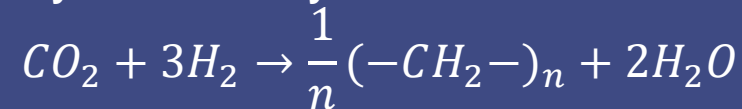
**Methanol synth. – TRL = 8**



→ **Thermodynamic control**  
(equilibrium X~25% at 250°C, 50 bar)

→ **Lower kinetics** (Cu or In catalysts)

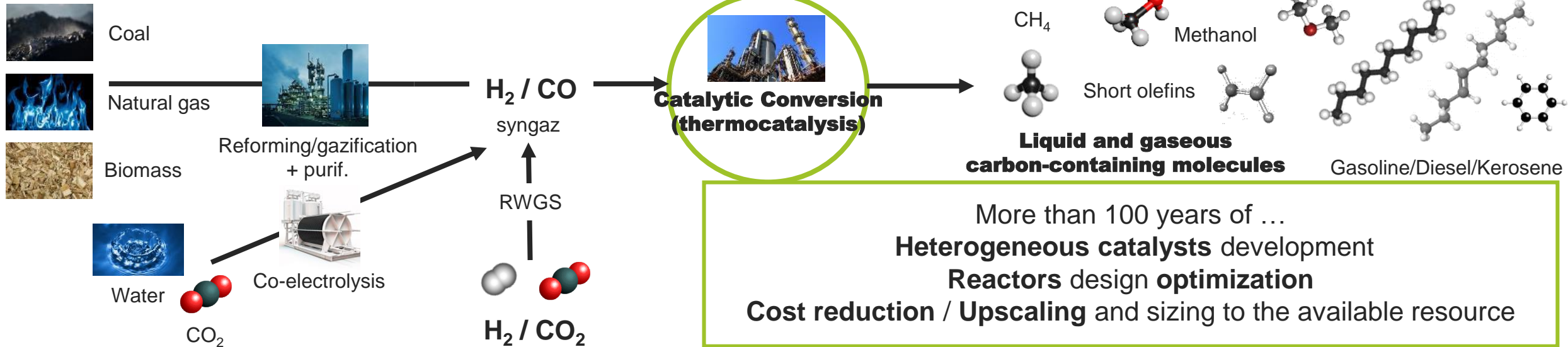
**Hydrocarbons synth. – TRL = 7 indirect / 3**



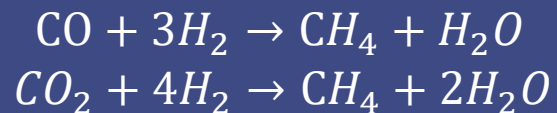
→ **Kinetic control** (no equilibrium)

→ **Limited selectivity** (syncrude)  
(Fe or Co catalysts)

# High maturity : history of technologies



## Methanation 1902 (Sabatier)



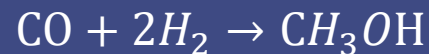
Paul Sabatier  
Nobel Prize 1912

CO euration in syngas for  $NH_3$  prod.

(1970 oil crisis) SNG from coal

(1980)  $CO_2$  méthanation

## Methanol synth. 1923 (Pier & Mittasch)



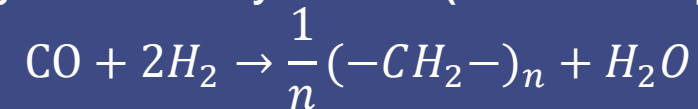
1<sup>st</sup> synthetic MeOH shipment  
BASF, Leuna, 1923

1<sup>st</sup> « low » pressure MeOH Plant  
ICI, 1966



(1990) Indirect  $CO_2$  MeOH synthesis

## Hydrocarbons synth. 1923 (Fischer & Tropsch)



1<sup>st</sup> Coal-to-Liquid Plant  
Ruhrchemie, Oberhausen, 1936

(1930) Coal-to-Liquid fuel (Germany)

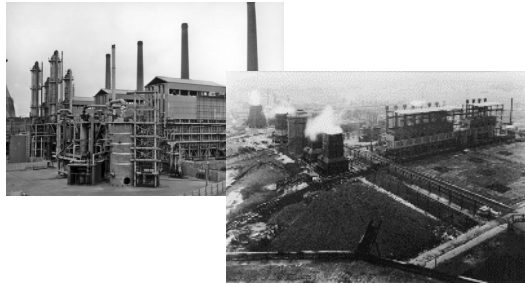
(1945-1970) Coal-to-Liquid fuel (USA)



(1990) Coal-to-Liquid (South Africa & China)  
+ Gas-to-Liquid (where Natural Gas available)

(2000) Biomass-to-Liquid / (2010) Power-to-Liquid



# But still R&D to be done




Feedstock available/storable in large quantity (C + energy source)  

Constant CO + H<sub>2</sub> inlet feed

Centralized ecosystem/infrastructures (pipes / harbours / networks)

Low costs (cheap fossil resources)

KPI = mainly costs €

Feedstock limited (biomass) or diluted (CO<sub>2</sub> in air)  Need of decarbonized energy sources (intermittency)

CO<sub>2</sub> or variable syngas (CO + CO<sub>2</sub> + H<sub>2</sub>) inlet feed

Decentralized usages / various sizes / multi-energy

Expensive electricity + CO<sub>2</sub> capture / H<sub>2</sub> production

KPI = CO<sub>2</sub> footprint + costs € / avoided CO<sub>2</sub>

LCA - environmental footprint : impact on soil, water, biodiversity

- Dynamic** behaviour of the **process** / management of **Stop&Go**
- New catalysts** development / **water tolerant** catalysts
- Modular** and **scalable reactors** and units
- Improve performances** to have the best use of electricity
- Multi-criteria analysis** for process selection

# Context of a process (example of methanation)

## Constraints (Upstream)

Energy availability



Quantity (power scale)  
Electrical Sources  
(on/off grid, intermittency)  
Heat availability

Hydrogen Resources



Water availability

Water quality (purification)

Carbon Resources



Quantity  
Quality (Purification)  
Stoichiometry

Land take  
Regulation

Social-acceptance  
Industrial landscape

Localization



Catalytic process



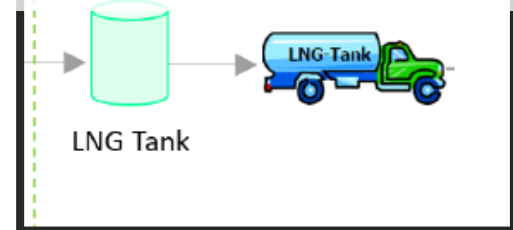
For each technologies :  
Adaptability,  
Flexibility  
Scale  
& process  
optimization/integration

## Applications (downstream)

Mobility (CNG)



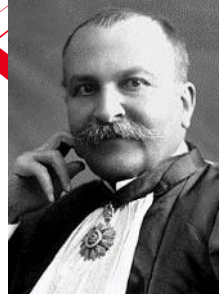
Energy transport (LNG)



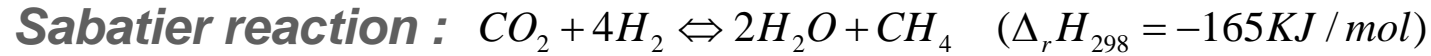
Grid injection



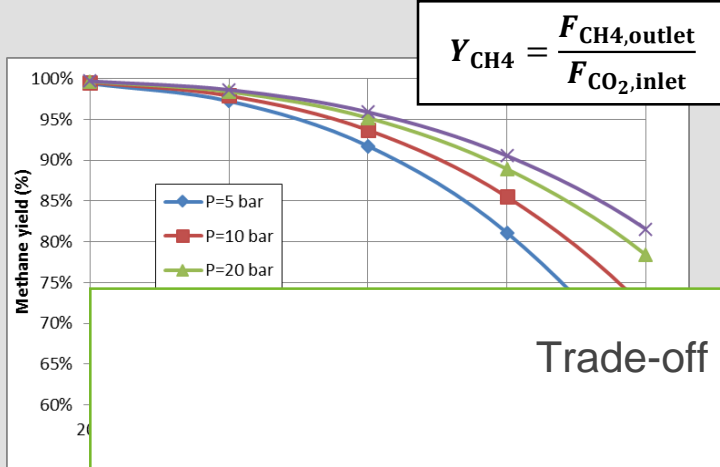
# Intrinsic methanation limitations



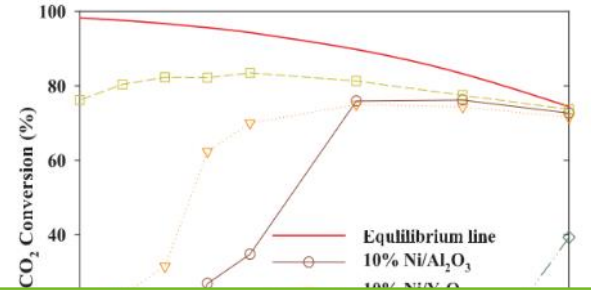
Paul Sabatier  
Nobel Prize 1912



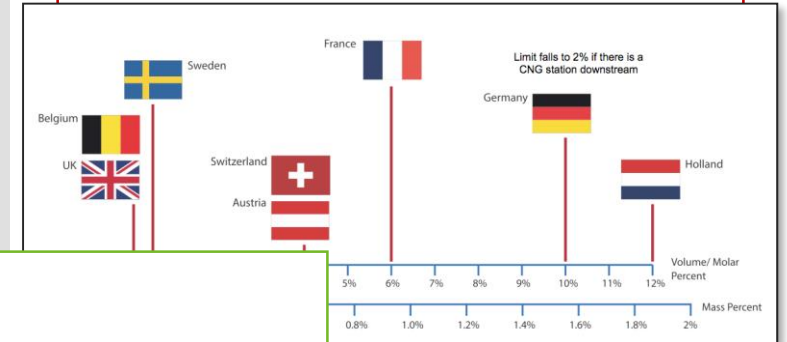
## Thermodynamics



## Kinetics



## Product specifications



Trade-off between Thermodynamics and Kinetics  
+ catalyst lifetime  
+ costs  
+ specs ...

( $H_2:CO_2 = 4:1$ )

J.Y. Ahn et al, Fuel 250 (2019) 277–284

grid  $H_2$  tolerance  
 $H_2 < 6 \text{ vol.}\%$  (now ~ 0 %),  
 $CO < 2 \text{ vol.}\%$

**Exothermal** → favored by **high P** and **low T**  
**Yield > 97%** for **T < 300°C**

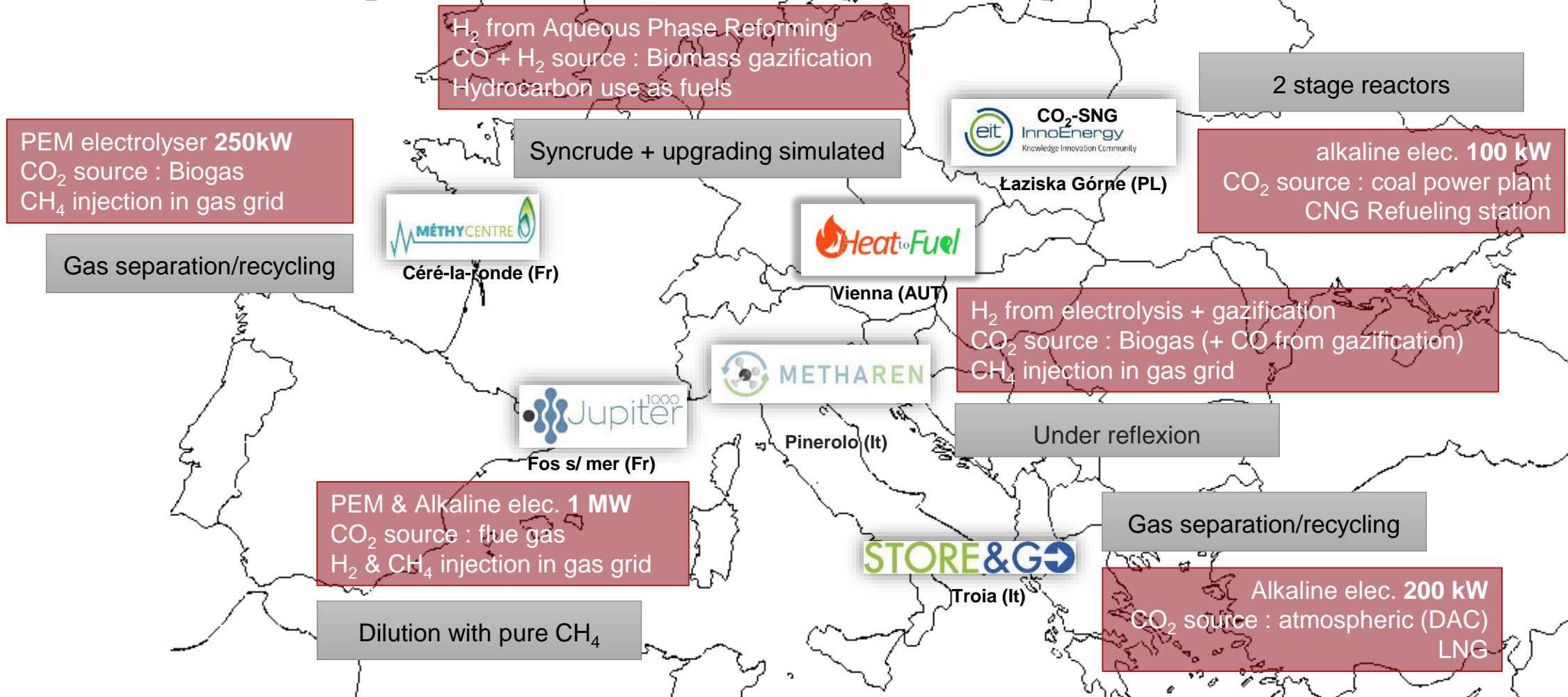
Catalyzed by **Ni active sites**  
→ **minimum activation temperature**

**T < 250°C**  
Active catalyst



Hard to reach in  
one reactor pass

# Few illustration of demo sites



# Any question ?



Parviz  
HAJIYEV



Vincent  
FAUCHEUX



Arthur  
ROUSSEY



Isabelle  
ROUGEAUX



Corentin  
CHATELIER



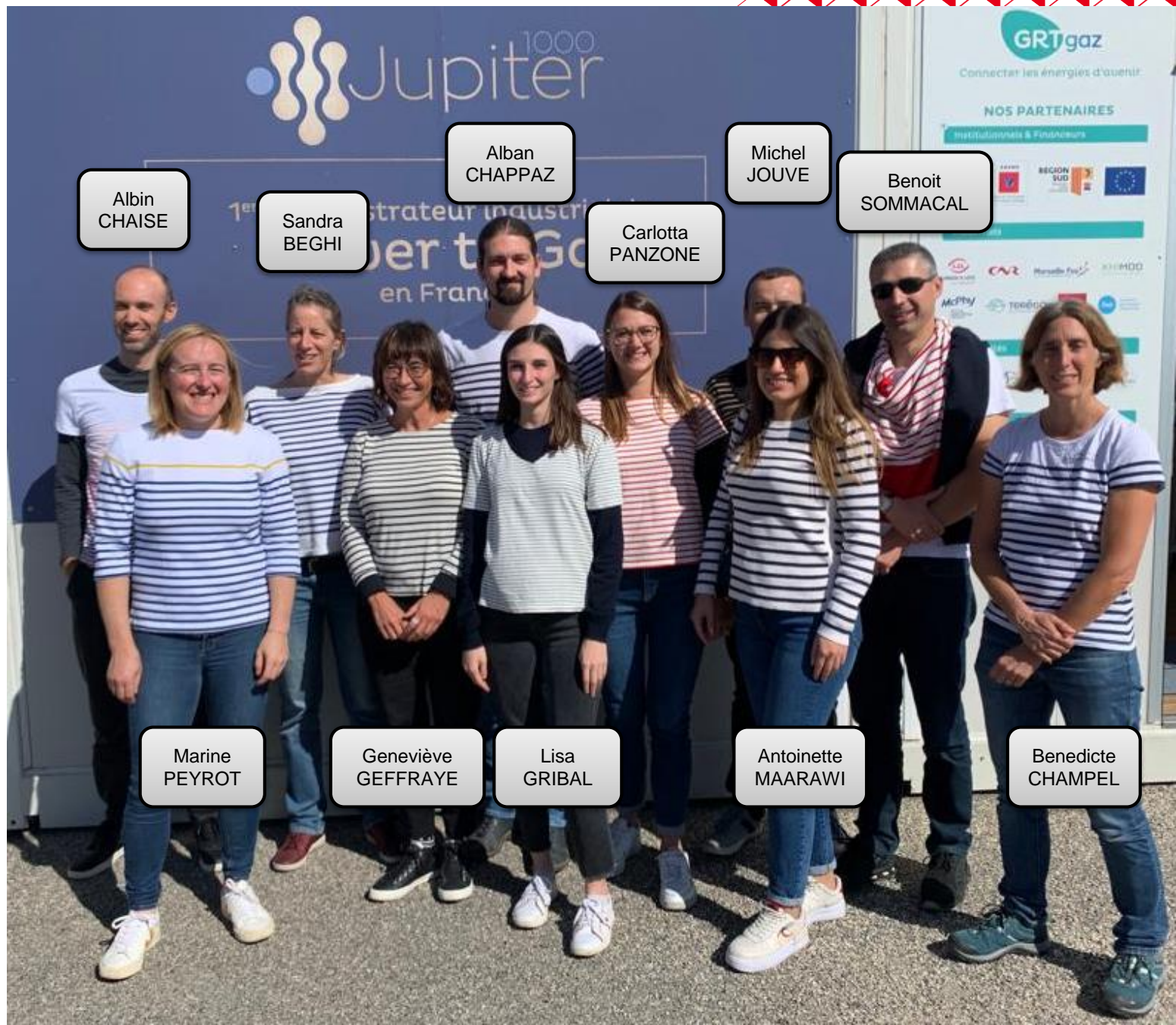
Konstantin  
TARASOV



Elhassan  
AMATERZ



ANDRÉ LUIZ  
ALVARENGA MARINHO



Albin  
CHAISE

Sandra  
BEGHI

Alban  
CHAPPAZ

Michel  
JOUVE

Benoit  
SOMMACAL

Carlotta  
PANZONE

Marine  
PEYROT

Geneviève  
GEFFRAYE

Lisa  
GRIBAL

Antoinette  
MAARAWI

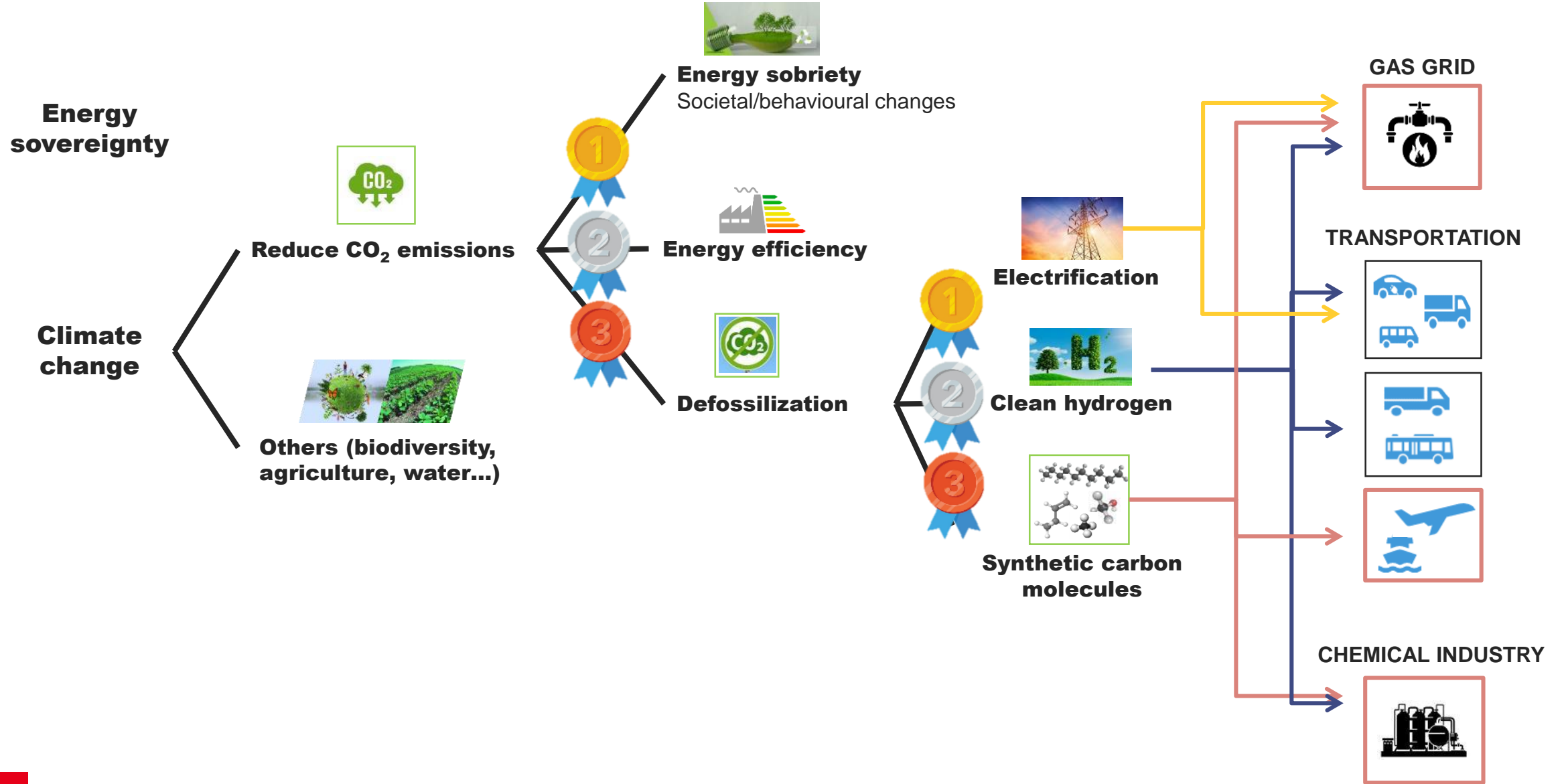
Benedicte  
CHAMPEL



# **3 ■ Energy efficiency Low duty vehicle case study**

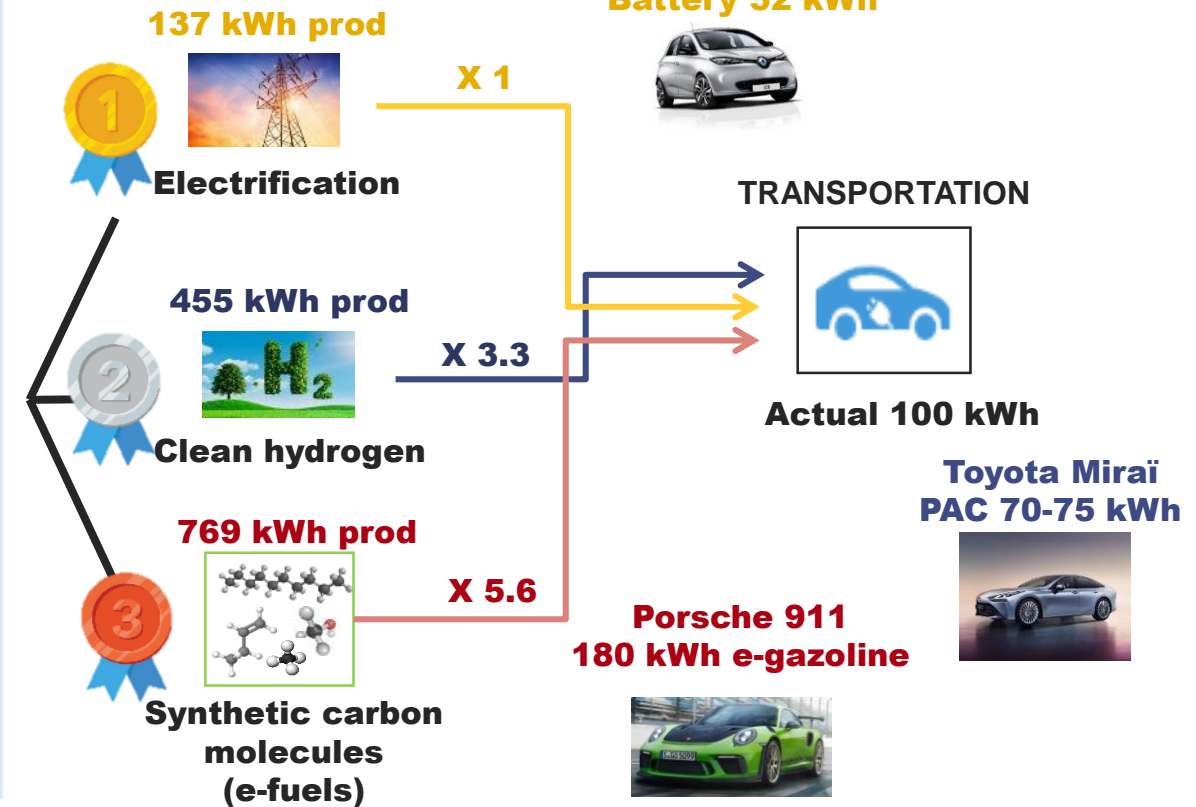
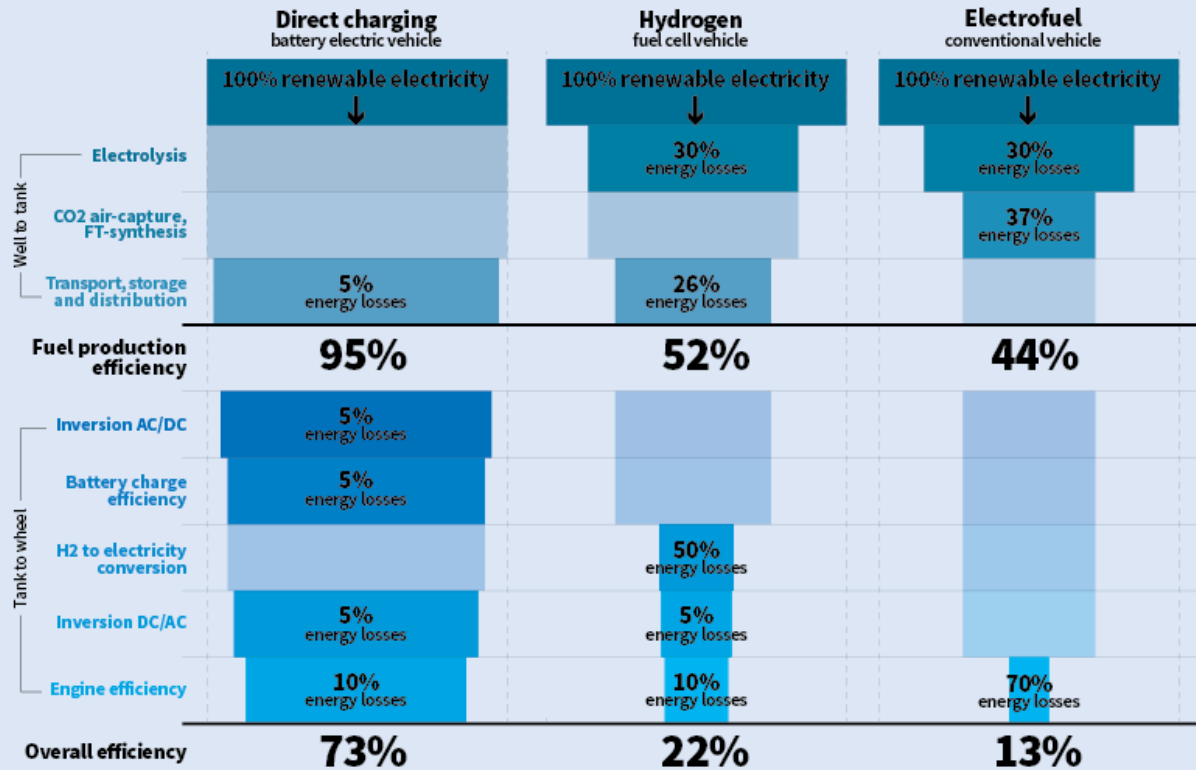


# Prioritization of solutions for climate change



# Efficiency of different pathways

## Energy efficiency of different technologies in a passenger car



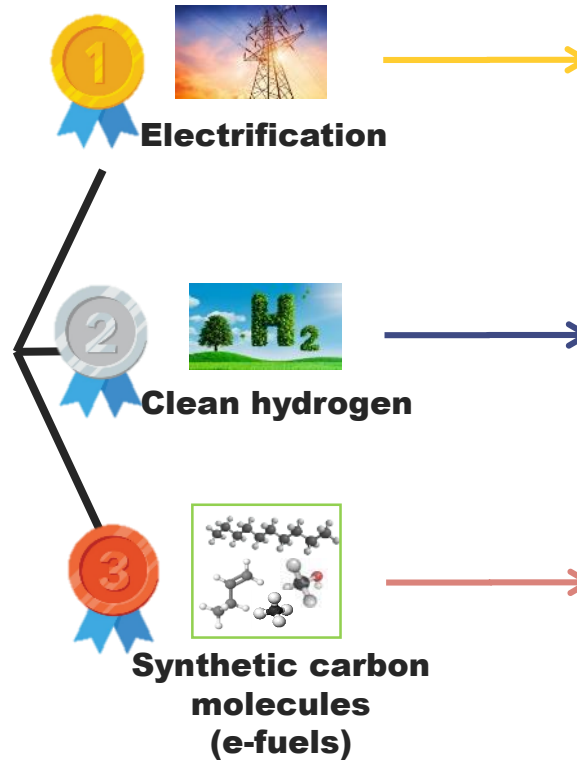
Carbon molecules will be needed in sectors where we don't have other choice → non-fossil sources of carbon molecules  
Where low carbon electricity is available

# Efficiency of different pathways

**Grand Place extension, Grenoble**  
**1730 m<sup>2</sup> PV panels → ~450 MWh annual production**



| Diesel         | Compressed Hydrogen 70 MPa | Lithium Ion Battery |
|----------------|----------------------------|---------------------|
| System Fuel    | System Fuel                | System Cell         |
| 43 kg<br>33 kg | 125 kg<br>6 kg             | 830 kg<br>540 kg    |
| 46 L<br>37 L   | 260 L<br>170 L             | 670 L<br>360 L      |



**12 Vehicles (~100 kWh)**  
**1 load./day**



**3.7 vehicles (~100 kWh)**  
**1 load./day**



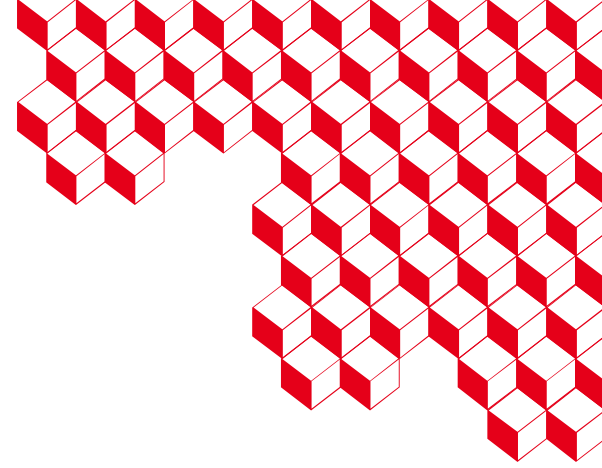
**2.2 Vehicles (~100 kWh)**  
**1 load./day**



**Carbon molecules will be needed in sectors where we don't have other choice → non-fossil sources of carbon molecules**



liten



**Thank you**

CEA-Liten, Grenoble, France

[liten.cea.fr](http://liten.cea.fr)

